# Heat, Mass, and Momentum Transfer Analogies for the Fully Developed Turbulent Flow of Power Law Fluids in Circular Tubes

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A new correlation is presented to describe heat and mass transfer at large Francti or Schmidt numbers to power law fluids in fully developed turbulent flow in a pipe. The resulting expression for the Stanton number differs from earlier semiempirical correlations in that it is based on a continuous eddy viscosity distribution from the wall to the center of the pipe and contains no adjustable parameters to be determined from heat transfer data. Nurselt numbers determined by the new correlation are in excellent agreement with data on heat transfer to both pseudoplastic and dilatent fluids.

Excellent reviews of the available correlations for heat and mass transfer to inelastic, time-independent, mon-Newtonian fluids in fully developed turbulent pipe flow are given by Metzner (18) and Skelland (31). The most widely used correlation to date has been that of Metzner and Friend (19), who extended the theoretical analogy of Reichardt (27) to purely viscous non-Newtonian fluids to obtain the following equation for the Nusselt number:

$$N_{Na} = \frac{f/2}{1.20 + c\sqrt{f/2}} N_{Re} N_{Fr}$$
 (1)

The parameters of the constitutive equation for the non-Newtonian fluid enter Equation (1) through the friction factor f, the non-Newtonian generalized Reynolds number  $N_{Be}$ , the generalized Prandtl number  $N_{Fe}$ , and the empirical function c, which in the general case also may be a function of the generalized non-Newtonian Reynolds number. These investigators determined c empirically from experimental heat transfer coefficients for both pseudoplastic and Newtonian fluids. Their final correlation has the form

$$N_{Nu} = \frac{f/2}{1.20 + 11.8 \sqrt{f/2} (N_{Prot} - 1) (N_{Prot})^{-1/2}} N_{Re} N_{Pr}$$
(2)

The Prandtl number at the wall  $N_{Prw}$  is related to the generalized Prandtl number as follows:

$$\frac{N_{Pr}}{N_{Pre}} = \left(\frac{16}{N_{Ref}}\right)^{\frac{n-1}{n}} \left(\frac{3n+1}{4n}\right)$$
(3)

In developing the above, the rheological behavior of the purely viscous non-Newtonian fluids was represented by the empirical Outwald-de Waele or power law constitutive equation

$$r = -\left\{K \left| \sqrt{\frac{1}{2} (\Delta : \Delta)} \right|^{n-1} \right\} \Delta \qquad (4)$$

This was chosen in view of its proved ability to portray experimental data over moderately large ranges of shear rate for many systems.

Equation (2) is restricted to nearly isothermal flow. Petersen and Christiansen (25) have extended Metzner and Friend's correlation to nonisothermal and transitional flow. These same authors have argued that the Frandti number to be used in Equation (2) should be corrected for the fact that the effective viscosity in the wall region is less than that in the turbulent core for pseudoplastic fluids, They suggest that the following effective Prandtl number be used in Equation (2):

$$N_{Pre} = \frac{808(n+2)^{(n+2)/(n+1)}}{1.085(3n+1)} N_{Pre}$$
 (5)

Clapp (4) extended Martinelli's (17) analogy to power law fluids. However, the Nusselt numbers predicted were considerably lower than those he observed for pseudoplastic fluids in the range 0.7 < n < 0.8. He proposed the empirical equation

$$N_{Nu} = 0.023 (9350)^{0.8(1-1/(u)^{a})} (N_{Re})^{0.8/(u)^{a}} (N_{Fe})^{0.4} (6)$$

Mizushina and Kuriwaki (20) recently correlated their heat transfer data on both pseudoplastic and dilatant fluids with a modified form of the Chilton-Colbum (3) equation:

$$N_{Nu} = (0.023)^{80u+20/1906u+103} - (N_{Nu})^{40u+20/1904u+103} (N_{Pr})^{1/2}$$
 (7)

Recently, Hughmark (10) has extended Longwell's (15) equation to power law fluids. The mean velocity profile is

# **Momentum Transfer In Fluids**

**C P Kothandaraman, R Rudramoorthy** 

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